

Powdery metal nanoparticle-based catalysts prepared by spark ablation for CO₂ methanation

P. Hongmanorom¹, D.P. Debecker^{1*}

¹Institute of Condensed Matter and Nanoscience, UCLouvain, Louvain-La-Neuve, Belgium

*damien.debecker@uclouvain.be

Introduction

Wet chemical methods are the most common processes implemented for both lab- and industrial-scale production of metal nanoparticles and supported metal nanoparticles. These processes usually generate large amounts of liquid waste, making use of solvents, ligands, surfactants, counter ions, etc. Also, they mostly rely on multi-step energy-intensive procedures, such as aging, drying, calcination, and reduction.¹ Spark ablation is a compelling alternative to traditional wet chemical methods, primed to reduced environmental impact (i.e., no use of solvents, precursors, salts, ligands, or high-temperature treatments). It was developed to generate nanoparticles, using electrical discharges between two electrodes of a target material in inert gas flow. This physical process yields primary metal particles in the 1-10 nm size range. The well-controlled deposition of generated metal nanoparticles onto flat surfaces has been well documented.^{2, 3} Yet, for heterogeneous catalysis, powdery materials are needed. We propose for the first time to modify a spark nanoparticle generator to allow a direct deposition onto pulverulent materials.⁴ The concept relies on the aerosolization of a powder, which is gas-transported and injected in the path of metal nanoparticle formation. Herein, TiO₂ powder is used as the catalyst support, while Ni electrodes are used to generate Ni nanoparticles as the active phase, forming the Ni/TiO₂ catalyst for CO₂ methanation.

Materials and Methods

In Figure 1 (Left), TiO₂ P25 (Degussa) powder was aerosolized from a mechanically vibrating reservoir by a 4-jet vortex fed with N₂ (99.9%; 3 L/min). The aerosolized powder was transported through a venturi for de-agglomeration before injection into the spark generator. Sparks generated between the Ni electrodes (99.99%; 3mm diameter) with a gap voltage of 1.3 kV and a charging current of 10.4 mA produced Ni clusters, which were carried by N₂ (99.9%; 3 L/min) to form Ni nanoparticles deposited onto TiO₂ particles. The resulting Ni/TiO₂ catalyst was collected on filter paper. The catalyst (200 mg) was reduced at 500°C for 2 h under a flow of 20 mL/min (50% H₂/50% He) prior to the reaction testing in the 200-400°C range with a gas mixture of 20 mL/min (10% CO₂ and 40% H₂ diluted in He). Catalyst characterization was performed using N₂ physisorption, H₂-TPR, XRD, ICP-AES, and HR-TEM.

Results and Discussion

The pristine TiO₂ support and the as-prepared Ni/TiO₂ catalyst exhibit a H3-type hysteresis loop, resulting from the interparticle voids in the loose aggregates of non-porous TiO₂ particles. After Ni loading (2.3 wt% determined by ICP-AES) and CO₂ methanation reaction, the TiO₂ diffraction peaks are unchanged in intensity, positions and width, which suggests that TiO₂ crystallites are unaffected by the catalyst preparation and reaction conditions. Additionally, the main diffraction peaks of Ni (2θ = 44.6°) or NiO (2θ = 43.1°) crystalline phases are not detectable

in the XRD pattern of the as-prepared Ni/TiO₂ catalyst, excluding the presence of Ni/NiO crystallites larger than 5 nm. TEM images further confirm this observation, showing many small Ni nanoparticles (<5 nm) well-dispersed on TiO₂. HRTEM images also reveal the lattice fringes with inter-planar distances of 2.0-2.1 Å and 2.35-2.45 Å, corresponding to the (111) crystal plane of cubic Ni and NiO, respectively. It should be noted that the homogeneity of the deposit is still not optimal, as some “floating” Ni/NiO nanoparticles can also be observed, not being in contact with TiO₂ support. Despite no interaction with TiO₂ support, these nanoparticles are very small (<5 nm). Although the Ni loading, Ni particle size and metal-support interaction have not been fully optimized, the Ni/TiO₂ catalyst achieves satisfactory CO₂ conversion of 53% and CH₄ selectivity of 76% at 400°C, as shown in Figure 1 (Right). After the reaction, HRTEM images show that small Ni nanoparticles (a few nanometer), well-dispersed on TiO₂ support, remain stabilized after reductive pretreatment and subsequent reaction. Nevertheless, few large particles (50-80 nm) can also be found, likely stemming from the sintering of “floating” Ni nanoparticles without interaction with TiO₂. The presence of few large Ni nanoparticles is consistent with the small and relatively narrow XRD peak at 44.6° of the spent Ni/TiO₂ catalyst. The homogeneity of deposition could be further improved by improving the design of the mixing zone and better controlling the powder aerosolization. Additionally, the scope could be expanded to other metals (e.g., Ru, Rh, Pd, Co, and Fe), which have been reported as active and selective metal catalysts for CO₂ methanation.

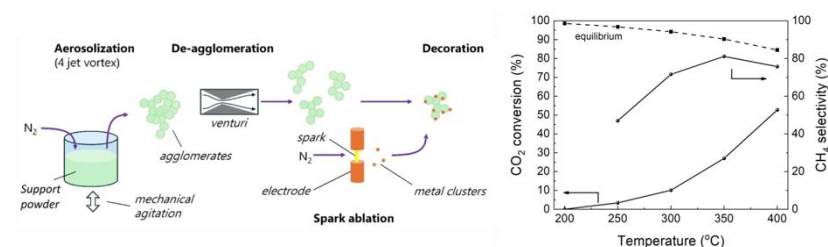


Figure 1. (Left) Schematic view on the set-up used to prepare powdery Ni/TiO₂ catalyst. (Right) CO₂ conversion and CH₄ selectivity of Ni/TiO₂ catalyst as a function of temperature.

Significance

We report the first synthesis of the powdery heterogeneous catalyst using spark ablation technology. The resulting Ni/TiO₂ catalyst is readily active in the hydrogenation of CO₂ to CH₄. This disclosed method opens new avenues for heterogeneous catalyst preparation.

References

1. N.D. Jaji, H.L. Lee, M.H. Hussin, H.M. Akil, M.R. Zakaria, M.B.H. Othman, *Nanotechnol. Rev.* **2020**, *9*, 1456.
2. T.V. Pfeiffer, J. Feng, A. Schmidt-Ott, *Adv. Powder Technol.* **2014**, *25*, 56.
3. S. Drdova, M. Gao, O. Sambalova, R. Pauer, Z. Zhou, S. Dimitriadou, A. Schmidt-Ott, J. Wang, *Environ. Sci.: Nano.* **2024**, *11*, 1023.
4. D.P. Debecker, P. Hongmanorom, T.V. Pfeiffer, B. Zijlstra, Y. Zhao, S. Casale, C. Sassoey, *Chem. Commun.* **2024**, *60*, 11076.